

Journal of Molecular Catalysis A: Chemical 150 (1999) 87-94



www.elsevier.com/locate/molcata

A novel palladium catalyst for the synthesis of hydrogen peroxide from carbon monoxide, water and oxygen

Daniele Bianchi *, Rossella Bortolo, Rino D'Aloisio, Marco Ricci

EniChem, Centro Ricerche Novara, Istituto G. Donegani, Via Fauser 4, I-28100 Novara, Italy

Received 22 December 1998; accepted 12 April 1999

Abstract

The synthesis of hydrogen peroxide from carbon monoxide, water and oxygen in a biphasic system using palladium complexes with bidentate nitrogen ligands as catalysts was investigated. After testing a series of phenanthroline derivatives, 2,9-dimethyl-4,7-diphenylphenanthroline (8) was selected as the most efficient ligand. The palladium complex with ligand 8 showed high stability and catalytic activity (turnover number up to 600 moles of hydrogen peroxide per mole of palladium per hour) and, on the basis of a preliminary study, carried out in continuous operation mode, it appears a promising catalyst for the development of an industrial process. © 1999 Elsevier Science B.V. All rights reserved.

Keywords: Palladium; N-ligands; Hydrogen peroxide

1. Introduction

Hydrogen peroxide is a chemical that is becoming more and more popular as an environmentally friendly oxidant, due mainly to its unique feature of producing water as the only by-product [1]. Industrially, hydrogen peroxide is produced primarily by the alternate oxidation and reduction of alkylantraquinone derivatives [2]. Since this method is quite complex (a stoichiometric amount of quinone must be used and recycled) extensive studies have been carried out in order to find a direct route, such as the synthesis from hydrogen and oxygen or from carbon monoxide, oxygen and water. The latter

* Corresponding author. E-mail:

daniele_bianchi@hq.enichem.geis.com

reaction, disclosed in 1979 by Yermakov et al. (Eq. (1)) [3], is less critical in terms of safety since it allows to operate in a wider range of non-ignitable gas phase composition.

$$O_2 + CO + H_2O \rightarrow H_2O_2 + CO_2 \tag{1}$$

Despite the favourable thermodynamics of the reaction ($\Delta G_{298}^{\circ} = -134 \text{ kJ mol}^{-1}$), the original catalyst (palladium triphenylphosphine complex) was quite inefficient and a turnover number (TON, moles of hydrogen peroxide per mole of palladium) of only 5 could be obtained. The fast catalyst inactivation was mainly due to the oxidation of the phosphine ligand with consequent precipitation of reduced palladium. A moderate improvement of the catalyst life (TON up to 87) was obtained by using the more stable triphenylarsine as the palladium ligand [4,5],

^{1381-1169/99/\$ -} see front matter 0 1999 Elsevier Science B.V. All rights reserved. PII: S1381-1169(99)00218-6

being the process still not suitable for a practical application.

On the other hand, during the last 15 years nitrogen ligands have turned out to be valuable substitutes of more traditional phosphorus ligands in a number of homogeneously catalysed reactions [6]. Recently, as a part of an industrial research aimed at developing a new process for the production of hydrogen peroxide, we have found that palladium complexes containing bidentate nitrogen ligands efficiently catalyse the reaction 1 with productivity quite comparable to that of the current commercial process [7]. Hydrogen peroxide formation is likely to occur through known reactions: (i) the reduction of Pd(II) complex, by carbon monoxide and water, affording carbon dioxide and Pd(0)species; (ii) the oxidation of this Pd(0) species by oxygen with formation of a Pd(II) peroxocomplex: (*iii*) the reaction of the latter species with an acid, producing hydrogen peroxide and restoring the initial Pd(II) complex.

We now report the influence of the reaction conditions (palladium ligand, acid cocatalyst, nature of the solvent, temperature and gas phase composition) on the hydrogen peroxide yield and the catalyst efficiency. We also report a study of the catalyst stability, carried out in continuous operation mode.

2. Experimental

The ligands used in this study were: 1,10phenanthroline (phen) (1), 2-2'-bipyridine (bipy) (2), 4,7-diphenyl-1,10-phenanthroline (4,7-dpphen) (3), 2,9-dimethyl-1,10-phenanthroline (2,9-dmphen) (4), 2,9-*n*-dibutyl-1,10-phenanthroline (2,9-dbphen) (5), 2,9-diphenyl-1,10phenanthroline (2,9-dphen) (6), 2,9-dichloro-1,10-phenantroline (2,9-dClphen) (7), 2,9-dimethyl-4,7-diphenyl-1,10-phenanthroline (2,9dm-4,7-dpphen) (8). Ligands 1–4 and 8 were purchased from Aldrich. Ligands 5, 6 and 7 were synthesised according to the procedures described in literature [8,9]. 2.1. General procedure for the synthesis of hydrogen peroxide (batch mode)

Pd(OAc)₂ (0.07 mmol), an acid (C₇F₁₅COOH or toluene-4-sulfonic) (2.8 mmol) and one among the ligands **1–8** (0.28 mmol) were dissolved in a mixture of the organic solvent (1,2,4-trichlorobenzene or toluene) (40 ml) and the cosolvent (1-butanol or 2-methyl-2-butanol) (60 ml), and stirred for 6 h at 25°C. The resulting complex solution was added to water (80 ml) to form a biphasic system and poured into an autoclave containing a glass liner. The reactor was then pressured to 6500 kPa partial pressure of O₂ and 600 kPa partial pressure of CO in order to form a non-flammable gas mixture.

The reactions were carried out for 1 h at 70°C, with the mixture being stirred by a magnetically-driven impeller. After depressuring the reactor, the hydrogen peroxide concentration in the aqueous solution was measured by titration with potassium permanganate.

2.2. Kinetic measurements

 $Pd(OAc)_2$ (2.5 mmol), $C_7F_{15}COOH$ (60 mmol) and 2,9-dm-4,7-dpphen (8) (20 mmol) were dissolved in a mixture of 1,2,4-trichlorobenzene (85 ml) and 2-methyl-2-butanol (15 ml). and stirred for 6 h at 25°C. Alternatively, a second catalytic system was prepared in the same way by using toluene-4-sulfonic acid and toluene instead of C₇F₁₅COOH and 1,2,4-trichlorobenzene, respectively. In both cases, the resulting solution was added to water (80 ml) to form a biphasic system. The comparison between the two catalysts was carried out in the same reactor described above, equipped with an automatic system to maintain constant the inlet pressure and composition of the gas mixture. The reactions were carried out at 70°C and 8100 kPa of total pressure ($P_{\rm CO} = 600$ kPa; $P_{\rm O_2} =$ 7500 kPa). The hydrogen peroxide concentration in the aqueous phase was determined periodically during the course of each run by temporarily stopping the gas flow for 1 min, which allowed the liquid phases to separate, withdrawing a measured volume of aqueous phase and pumping back into the reactor an equal volume of deionised water.

2.3. Synthesis of hydrogen peroxide (continuous operation mode)

 $Pd(OAc)_2$ (2.5 mmol), toluene-4-sulfonic acid (60 mmol) and 2,9-dm-4,7-dpphen (8) (20 mmol) were dissolved in a mixture of toluene (85 ml) and 2-methyl-2-butanol (15 ml), and stirred for 6 h at 25°C. The resulting solution was added to water (80 ml) to form a biphasic system.

The reaction was carried out in a stainless steel (Hastellov C) autoclave equipped with a bottom outlet and an automatic system to maintain constant the inlet pressure and composition of the gas mixture. The reactor was fed with an aqueous solution of toluene-4-sulfonic acid (87 mM) and hydrochloric acid (1 mM), saturated with 2-methyl-2-butanol. The aqueous phase (containing the produced hydrogen peroxide) was selectively withdrawn from a non-stirred area created on the bottom of the reactor which allowed the phase separation. The feeding and withdrawal flow rate were 80 ml/h corresponding to a residence time of 1 h. The reaction was carried out at 70°C and 8100 kPa of total pressure ($P_{CO} = 600 \text{ kPa}$; $P_{O_2} = 7500 \text{ kPa}$) for 10 h in a continuous operation mode.

3. Results and discussion

The reaction was carried out in a biphasic system, being the catalyst soluble in the organic phase and the produced hydrogen peroxide soluble in the aqueous phase. The biphasic operation minimises the ligand oxidation by reducing the contact with hydrogen peroxide and makes possible the separation and recycling of the catalyst by simple decantation. After screening a wide variety of organic solvents, we found that the reaction was strongly accelerated by the presence of a water-immiscible alcohol which possibly plays an active role in the reaction mechanism, acting as a ligand itself.

The selected reaction medium, for the catalysts comparison, was a mixture of 1-butanol, 1,2,4-tricholorobenzene (a hydrophobic solvent added in order to improve the phase separation) and water. The catalysts were generated in situ from Pd(acetate)₂, 4 equiv of one among the ligands **1–8**, and 40 equiv of sulfuric acid, added as a cocatalyst. All the reactions were performed at 70°C and 7100 kPa of total pressure with an excess of oxygen ($P_{\rm CO} = 600$ kPa; $P_{\rm O_2} = 6500$ kPa) in order to prevent the precipitation of reduced palladium, which becomes predominant under reducing conditions.

As reported in Table 1, we observed three different reactivities, depending on the nature of the substitution in the 2,9-positions of the ligand. All the unsubstituted ligands phen (1), bipy (2) and 4,7-dpphen (3), in presence of CO, lead to the formation of stable red complexes, being as a result ineffective in the synthesis of hydrogen peroxide.

The ligands bearing bulky substituents, such as 2,9-dbphen (5) and 2,9-dpphen (6), due to their steric hindrance adjacent to the N-donor function, do not form stable species but gave

Table 1 Effect of the ligand^a

Acid	$TOF(h^{-1})^b$	
H_2SO_4	0 ^c	
H_2SO_4	$0^{\rm c}$	
H_2SO_4	$0^{\rm c}$	
H_2SO_4	4^{d}	
H_2SO_4	$0^{\rm c}$	
H_2SO_4	$0^{\rm e}$	
H_2SO_4	32	
H_2SO_4	431	
	Acid H ₂ SO ₄ H ₂ SO ₄	Acid TOF $(h^{-1})^b$ H_2SO_4 0^c H_2SO_4 32 H_2SO_4 431

^aLigand/acid/Pd molar ratio: 4/40/1; solvent: trichlorobenzene/1-butanol/water 35/25/40 (v/v/v); temperature: 70°C; P_{CO} : 600 kPa; P_{O} : 6500 kPa.

^bTurnover frequency (moles of hydrogen peroxide per mole of palladium per hour).

^cThe formation of stable red complexes was observed.

^dThe complex was soluble in the aqueous phase.

^eThe precipitation of reduced palladium was observed.

Table 2 Effect of the acid promoter^a

-			
Ligand	Acid	$TOF(h^{-1})^b$	
2,9-dm-4,7-dpphen (8)	H_2SO_4	431	
2,9-dm-4,7-dpphen (8)	Tol-SO3H	442	
2,9-dm-4,7-dpphen (8)	HC1	0	
2,9-dm-4,7-dpphen (8)	HPF_6	172 ^c	
2,9-dm-4,7-dpphen (8)	CF ₃ COOH	528	
2,9-dm-4,7-dpphen (8)	C ₇ F ₁₅ COOH	634	
2,9-dm-4,7-dpphen (8)	C ₈ F ₁₇ SO ₃ H	170 ^c	
2,9-dmphen (4)	H_2SO_4	4	
2,9-dmphen (4)	C ₇ F ₁₅ COOH	681	

^aLigand/acid/Pd molar ratio: 4/40/1; solvent: trichlorobenzene/1-butanol/water 35/25/40 (v/v/v); temperature: 70°C; P_{CO} : 600 kPa; $P_{O_{2}}$: 6500 kPa.

^bTurnover frequency (moles of hydrogen peroxide per mole of palladium per hour).

^cThe precipitation of reduced palladium was observed.

unstable Pd(0) complexes which quickly dissociated with formation of reduced palladium. The best results were obtained with 2,9-dm-4,7-dpphen (8), which showed the optimum steric and donating capacity for the palladium catalysed synthesis of hydrogen peroxide. The lower turnover frequency (TOF) found for the 2,9dClphen (7) indicates that such electronwithdrawing substituents have a severe negative effect on the catalytic activity, while 2,9-dmphen (4) afforded a water soluble complex, almost inactive under these reaction conditions.

In addition to the above described phenanthroline derivatives, we tested a series of monodentate (triphenylamine, 4-phenylpyridine, 2, 6-dicholoropyridine, phenanthridine) and polydentate nitrogen ligands [2,6-di(2-pyridil)pyridine, 2,3-di(2-pyridil)pyrazine, 3,6-di(2-pyridil)-1,2,4,5-tetrazine, 6,7-dimethyl-2,3-di(2pyridyl)quinoxaline, 2,4,6-tri(2-pyridil)triazine, picolinic acid] without finding any appreciable activity in the synthesis of hydrogen peroxide.

The same set of ligands was used for an extensive screening of different metals (Fe, Ru, Co, Rh, Ir, Ni, Pt, Cu, Ag), in order to find a possible alternative to the palladium. Operating in the same reaction conditions, only a slight activity (TOF = 5) was detected using the platinum complex with ligand **8**, whereas all the

other metals gave inactive species confirming the unique features of palladium as a catalyst.

As shown in Table 2 for the palladium complex with ligand 8, an improvement of the catalyst efficiency was obtained by using an acid promoter, such as trifluoroacetic or perfluorooctanoic acid, the anion of which coordinates only weakly to the metal. In the case of the perfluorooctanoic acid, even the water soluble palladium complex formed with the hydrophilic ligand 4 was moved into the organic phase by the highly hydrophobic anion acting as a phase transfer agent (the partition of the complex in the organic phase was < 1% and > 99%with trifluoroacetate and perfluorooctanoate anion, respectively), showing a dramatic raising of TOF from 4 to 681 h^{-1} . Other fluorinated acids. such as perfluorooctanesulfonic and hexafluorophosporic acids, accelerated the dissociation of the complex with precipitation of reduced palladium. Conversely, the strongly coordinating chloride anion inhibited the reaction by forming stable unreactive complexes.

In Fig. 1, the effect of the temperature on the catalytic activity of the complex with ligand **8** is reported. A sharp increase of TOF was measured in the temperature range between 0 and 70° C. The process was not carried out at higher



Fig. 1. Effect of the temperature. Ligand $8/C_7F_{15}$ COOH/Pd molar ratio: 4/40/1; solvent: trichlorobenzene/1-butanol/water 35/25/40 (v/v/v); total pressure: 7100 kPa (P_{CO} : 600 kPa; P_{O_3} : 6500 kPa).

temperature in order to prevent side reactions such as the hydrogen peroxide decomposition and the ligand oxidation.

The study of the effect of the gas phase composition on the catalyst activity and stability was carried out by operating with non-ignitable mixtures of oxygen and carbon monoxide below the Lower Explosion Limit (LEL = 12.5% CO molar fraction) and above the Upper Explosion Limit (UEL = 94% CO molar fraction).

As shown in Fig. 2, under oxidising conditions the reaction was accelerated by increasing the carbon monoxide molar fraction up to 9%; beyond this value the complex became unstable and partial precipitation of reduced palladium started to occur. This phenomenon was emphasised operating under reducing conditions (98% CO molar fraction) where the immediate precipitation of reduced palladium was observed with production of traces of hydrogen peroxide.

As reported above, the selection of the most efficient catalysts was carried out in a biphasic system using a mixture of 1-butanol and 1,2,4trichlorobenzene (2:3 v:v) as organic phase. As shown in Table 3, the presence of the alcohol cosolvent was necessary to activate the reduction of the palladium complexes, which was completely unreactive in pure trichlorobenzene,



Fig. 2. Effect of the gas-phase composition. Ligand $8/C_7F_{15}$ COOH/Pd molar ratio: 4/40/1; solvent: trichlorobenzene/1-butanol/water 35/25/40 (v/v/v); temperature: 70°C; total pressure: 7100 kPa. (*) LEL: Lower Explosion Limit for carbon monoxide/oxygen mixtures.

Table 3 Effect of the alcohol cosolvent^a

Ligand	Cosolvent	% cosolvent ^b	$TOF(h^{-1})^{c}$
2,9-dm-4,7-dpphen (8)	none	0	0
2,9-dm-4,7-dpphen (8)	1-butanol	40	634
2,9-dm-4,7-dpphen (8)	1-butanol	100	15 ^d
2,9-dm-4,7-dpphen (8)	2-methyl-2-	40	578
	butanol		
2,9-dmphen (4)	none	0	0
2,9-dmphen (4)	1-butanol	40	681
2,9-dmphen (4)	2-methyl-2-	40	124
	butanol		

^aLigand/C₇F₁₅COOH/Pd molar ratio: 4/40/1; solvent: trichlorobenzene/alcohol/water; temperature: 70°C; P_{CO} : 600 kPa; P_{O_2} : 6500 kPa.

^bCosolvent/trichlorobenzene v/v ratio.

^c Turnover frequency (moles of hydrogen peroxide per mole of palladium per hour).

^dThe precipitation of reduced palladium was observed.

whereas it was rapidly reduced to Pd-black operating in pure 1-butanol.

The analysis of the solvent at the end of the reaction revealed that 1-butanol was partially oxidised to butanal (2% conversion was found after 10 h). A comparative test, carried out in absence of carbon monoxide, showed that primary and secondary alcohols can act themselves as reducing agents of the palladium [10], with formation of hydrogen peroxide and the corresponding carbonyl derivative, according to Eq. (2).

$$O_2 + R_2 CHOH \rightarrow H_2 O_2 + R_2 CO$$
 (2)

The reaction is catalysed by the palladium complex since 1-butanol does not undergo spontaneous oxidation under the given reaction conditions.

This side reaction could be avoided by using a tertiary alcohol cosolvent (2-methyl-2-butanol) which was equally effective at least in the activation of the complex with the ligand $\mathbf{8}$ and resulted in stability toward the palladium catalysed oxidation.

An equally crucial role in determining the catalytic activity and the stability of the catalyst was played by the organic solvent present as the second component of the organic medium.

In Table 4 are reported the turnover numbers and the residual catalytic activities of the complex with the ligand 8. measured after 3 h of reaction in different organic media. The residual activity was determined by recycling the organic phase in a successive catalytic cycle, after removal of the aqueous phase containing the produced hydrogen peroxide and replacing with an equal amount of pure water. In spite of their strong accelerating effect on the synthesis of hydrogen peroxide (Table 4, entries 1, 4), chlorinated solvents caused a rapid inactivation of the catalyst. Only a negligible improvement of the catalyst stability was obtained, replacing the perfluorinated acid with the non-halogenated toluene-4-sulfonic acid (entry 2), indicating the prevailing effect of the solvent.

This phenomenon was explained by the presence of an undesired side-reaction: the reduction of the organic chloride catalysed by the palladium with carbon monoxide and water, according to Eq. (3).

$$RCl + CO + H_2O \rightarrow RH + HCl + CO_2$$
 (3)

Using 1,2,4-tricholobenzene as a solvent, a progressive accumulation of mono- and dichlorobenzenes was indeed detected in the reaction mixture by GLC-MS analysis. The hydrochloric acid generated in this way, even at a

Table 4	
Effect of chlorinated	solvents



Fig. 3. Synthesis of hydrogen peroxide by palladium catalysis: kinetic profile. (\Box) Ligand **8**; acid: C₇F₁₅COOH; solvent: 2,4-trichlorobenzene/2-methyl-2-butanol/water; (\blacksquare) Ligand **8**; acid: toluene-4-sulfonic acid; solvent: toluene/2-methyl-2butanol/water; Pd/Cl⁻ molar ratio: 1/1. Temperature: 70°C; total pressure: 8100 kPa ($P_{CO} = 600$ kPa; $P_{O_2} = 7500$ kPa).

low concentration (molar ratio Cl/Pd \ge 4/1), can act as a strongly coordinating ligand of palladium, leading to the formation of stable complexes with consequent irreversible inactivation of the catalyst [11]. The higher the observed chloride release rate (1,2-dichloroethane > trichlorobenzene > chlorobenzene), the faster the inactivation rate of the catalyst (entries 2–4).

The mass spectroscopy analysis of the exhausted catalyst, recovered from a chlorinated

Effect of emolimated solvents					
Entry	Solvent	Acid	TON ^b	Residual catalytic activity (%) ^c	
1	1,2,4-trichlorobenzene	C ₇ F ₁₅ COOH	939	31	
2	1,2,4-trichlorobenzene	Tol-SO ₃ H	658	35	
3	chlorobenzene	Tol-SO ₃ H	738	57	
4	1,2-dichloroethane	Tol-SO ₃ H	251	0	
5	toluene	C ₇ F ₁₅ COOH	293	69^{d}	
6	toluene	Tol-SO ₃ H	42	0^{d}	
7	toluene ^e	C ₇ F ₁₅ COOH	420	100	
8	toluene ^c	Tol-SO ₃ H	876	100	

^aLigand 8/acid/Pd molar ratio: 4/40/1; solvent: 2-methyl-2-butanol/water 35/25/40 (v/v/v); temperature: 70°C; P_{CO} : 600 kPa; P_{O_2} : 6500 kPa.

^bTurnover number (moles of hydrogen peroxide per mole of palladium after 3 h of reaction).

^cMeasured after 3 h of reaction.

^dThe precipitation of reduced palladium was observed.

^eA weighed amount of hydrochloric acid was added to the reaction mixture with a molar ratio Cl/Pd = 1/1.

D. Bianchi et al. / Journal of Molecular Catalysis A: Chemical 150 (1999) 87-94

reaction medium (tricholorobenzene/2-methyl-2-butanol), revealed indeed the presence of chlorine containing polynuclear species with molecular weight higher than 1000.

The attempt to replace halogenated solvents with toluene were initially unsuccessfully (entry 5, 6), since in the chloride-free medium the complex became unstable and the rapid precipitation of reduced palladium was detected. A similar behaviour was observed with a series of different non-chlorinated solvents such as xylene, anisole, acetophenone and benzonitrile.

Much better results, in terms of catalyst stability, were obtained operating in the halogenfree solvent, adding only a weighed amount of hydrochloric acid (Cl:Pd molar ratio = 1:1), which exerted a remarkable stabilising effect against the formation of reduced palladium [12] (entry 7, 8).

In Fig. 3 are reported the kinetic profiles of the reaction carried out using the ligand **8** operating either in a halogenated environment (acid: $C_7F_{15}COOH$; solvent: 1,2,4-trichlorobenzene/ 2-methyl-2-butanol/water) and in a halogenfree environment (acid: toluene-4-sulfonate, solvent: toluene/2-methyl-2-butanol/water). Under the latter conditions it was possible to achieve high TON, producing hydrogen peroxide aqueous solutions up to 8% w/w concentration.

The stability of the catalytic system was confirmed with a preliminary test in continuous operation mode. In this case, the aqueous phase, containing the produced hydrogen peroxide, was continuously withdrawn from the bottom of the reactor while an aqueous solution of toluene-4sulfonic acid and hydrochloric acid, saturated with 2-methyl-2-butanol, was fed from the top, as described in Section 2. The catalyst, quantitatively distributed in the organic phase, was maintained inside the reactor. As shown in Fig. 4, the hydrogen peroxide productivity was constant for 10 h of operation (H₂O₂ concentration in the aqueous phase = 1.8% w/w; TON = 1600), without any appreciable loss of the catalytic activity.



Fig. 4. Synthesis of hydrogen peroxide by palladium catalysis: continuous operation. Ligand **8**; acid: toluene-4-sulfonic acid; solvent: toluene/2-methyl-2-butanol/water; Pd/Cl⁻ molar ratio: 1/1. Temperature: 70°C; total pressure: 8100 kPa ($P_{\rm CO} = 600$ kPa; $P_{\rm O_2} = 7500$ kPa). (\blacksquare) Hydrogen peroxide concentration in the aqueous phase withdrawn from the reactor; (*) turnover number (moles of hydrogen peroxide per mole of palladium).

In conclusion, complexation of palladium with a suitable bidentate nitrogen ligand provides an efficient catalyst for the synthesis of hydrogen peroxide from carbon monoxide, oxygen and water. The structure of the ligand as well as the nature of the weakly-coordinating anion and the solvent play a key role in determining the catalytic activity and the operational stability of the complexes, which were both dramatically improved with respect to the palladium-based catalytic systems already described in literature. The development of a continuous operation process, more suitable for an industrial application, is presently under consideration.

References

- G. Strukul, in: G. Strukul (Ed.), Catalytic Oxidations with Hydrogen Peroxide as Oxidant, Kluver, Dordrecht, 1992, p. 1.
- [2] G. Goor, in: G. Strukul (Ed.), Catalytic Oxidations with Hydrogen Peroxide as Oxidant, Kluver, Dordrecht, 1992, p. 13.
- [3] V.N. Zudin, V.A. Likholobov, Y.I. Yermakov, Kinet. Katal. 20 (1979) 1559.
- [4] F.E. Jacobson, (BOC) U.S. Patent, 4711772, 1987.
- [5] F.E. Jacobson, Chem. Abstr. 108 (1988) 40590x.

- [6] A. Togni, L.M. Venanzi, Angew. Chem., Int. Ed. Engl. 33 (1994) 497.
- [7] D. Bianchi, R. Bortolo, R. D'Aloisio, M. Ricci, Angew. Chem. Int. Ed. Engl. 33 (1999) 706.
- [8] C.O. Dietrich-Buchecker, P.A. Marnot, J.P. Savage, Tetrahedron Lett. 50 (1982) 5291.
- [9] M. Yamada, Y. Nakamura, S. Kuroda, I. Shimao, Bull. Chem. Soc. Jpn. 63 (1990) 2710.
- [10] K.P. Peterson, R.C. Larock, J. Org. Chem. 63 (1998) 3185.
- [11] A. Bontempi, E. Alessio, G. Chanos, G. Mestroni, J. Mol. Catal. 42 (1987) 67.
- [12] F. Ragaini, S. Cenini, J. Mol. Catal. A: Chem. 109 (1996) 1.